

A mixture theory analysis for passive transport in osmotic loading of cells

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Abstract

The theory of mixtures is applied to the analysis of the passive response of cells to osmotic loading with neutrally charged solutes. The formulation, which is derived for multiple solute species, incorporates partition coefficients for the solutes in the cytoplasm relative to the external solution, and accounts for cell membrane tension. The mixture formulation provides an explicit dependence of the hydraulic conductivity of the cell membrane on the concentration of permeating solutes. The resulting equations are shown to reduce to the classical equations of Kedem and Katchalsky (Biochem. Biophys. Acta 27 (1958) 229, J. Gen. Physiol. 45 (1961) 143) in the limit when the membrane tension is equal to zero and the solute partition coefficient in the cytoplasm is equal to unity. Numerical simulations demonstrate that the concentration-dependence of the hydraulic conductivity is not negligible; the volume response to osmotic loading is very sensitive to the partition coefficient of the solute in the cytoplasm, which controls the magnitude of cell volume recovery; and the volume response is sensitive to the magnitude of cell membrane tension. Deviations of the Boyle–van't Hoff response from a straight line under hypo-osmotic loading may be indicative of cell membrane tension.

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1. Introduction

The fundamental physical mechanisms of solute and water transport across the cell membrane have long been studied in the field of cell membrane biophysics, and there exist a number of formalisms aiming to characterize transport through membrane channels and/or lipid bilayers. These formalisms include a one-parameter (solute permeability) model (Mazur et al., 1974), a classic two-parameter (water and solute permeability) model (Jacobs and Stewart, 1932) and a commonly used three-parameter model (water and solute permeability and a solute–solvent interaction term) developed by Kedem and Katchalsky (1958). The parameters of interest (permeabilities) can be extracted

from the formulation when the cell volume change is measured in the experiment, assuming that the cell volume change is due purely to the volume of the water (and solute) that enters or exudes from the cell. These formulations have been derived from the general theory of irreversible thermodynamics (Onsager, 1931a, b; Staverman, 1952).

In more recent decades, the field of rational mechanics has addressed problems in the mixture of fluids (solvent and solutes) (Mills, 1966) as well as the mixture of fluids and solids (deformable porous media) (Atkin and Craine, 1976; Bowen, 1980; Mow et al., 1980; Frank and Grodzinsky, 1987; Lai et al., 1991; Huyghe and Janssen, 1997; Gu et al., 1998). In this study we propose to apply the theory of mixtures to the analysis of the passive response of cells to osmotic loading. For ease of comparison with the more classical treatment of Kedem and Katchalsky (1958, 1961), the analysis is limited to non-electrolytes. However, the formulation is

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Nomenclature

a	cell radius	p_e	fluid pressure in external solution
A	cell surface area	p_i	fluid pressure in cytoplasm
c^α	concentration of solute α inside the mixture, on a solvent volume basis	P^α	membrane permeability of solute α
c_0^α	concentration of solute α in the standard state	R	universal gas constant
\bar{c}^α	average concentration of solute α inside the membrane	T	surface tension in membrane
c_e^α	concentrations of solute α in external solution	V	cell volume
c_i^α	concentration of solute α in cytoplasm	\mathbf{v}^α	velocity of constituent α
D^α	solute diffusivity in mixture of solid and fluid	$\alpha = n$	refers to non-permeating solute
D_0^α	solute diffusivity in free solution	$\alpha = p$	refers to permeating solute
\mathbf{F}	deformation gradient of the solid matrix	$\alpha = s$	refers to solid matrix
$f_{\alpha\beta}$	diffusive drag coefficient between constituents α and β	$\alpha = w$	refers to solvent
J^w	volume flux of solvent across membrane	φ^α	volume fraction of constituent α in the mixture
J^α	molar flux of solute α across membrane	φ_i^w	volume fraction of osmotically active water in the cell
k	hydraulic permeability of solid matrix to pure solvent	κ^α	partition coefficient of solute α inside mixture relative to free solution
\tilde{k}	hydraulic permeability of solid matrix to solution (solvent + solutes)	κ_i^α	partition coefficient of solute α between cytoplasm and external solution
L_p	membrane hydraulic conductivity (or conductance)	$\tilde{\mu}^\alpha$	chemical potential of solvent ($\alpha = w$) or solute
M_α	molecular weight of solute α	μ_0^α	chemical potential of constituent α in the standard state
n_i^α	number of moles of solute α inside the cell	ρ^α	apparent density of constituent α
p	fluid pressure inside the mixture	ρ_T^w	true density of solvent
		θ	absolute temperature
		$\boldsymbol{\sigma}^e$	effective stress tensor in solid matrix
		σ_{rr}^e	normal effective stress in radial direction
		σ^α	Staverman's reflection coefficient for solute α

generalized to multiple solute species; it also incorporates partition coefficients for the solutes in the cytoplasm relative to the external solution, and accounts for cell membrane tension.

2. Methods

In this analysis the cell is modeled as a fluid-filled membrane, where the membrane is described by the mixture theory equations presented below. These equations are generally valid for neutral solute transport in uncharged porous media. In the following sections, the general equations of mixture theory are reduced to the case of a thin membrane, specialized to the case of one permeating and one non-permeating solute, and then compared to the classical Kedem–Katchalsky (K–K) model.

2.1. Governing equations of mixture theory

In the presentation of the mixture theory equations we use the notation of Gu et al. (1998), along with the

generalizations to the solvent and solute momentum equations and solute constitutive equation as described by Mauck et al. (2003). The mixture consists of a solid matrix ($\alpha = s$), solvent ($\alpha = w$) and solutes ($\alpha \neq s, w$), with each constituent assumed to be intrinsically incompressible and neutrally charged. The momentum equations for the mixture as a whole and for the solvent and solutes are given respectively by

$$-\text{grad } p + \text{div } \boldsymbol{\sigma}^e = \mathbf{0}, \quad (1)$$

$$-\rho^\alpha \text{grad } \tilde{\mu}^\alpha + \sum_{\beta} f_{\alpha\beta} (\mathbf{v}^\beta - \mathbf{v}^\alpha) = \mathbf{0}, \alpha \neq s, \quad (2)$$

where p is the fluid (solution) pressure, $\boldsymbol{\sigma}^e$ is the effective (or elastic) stress in the solid matrix, $\tilde{\mu}^\alpha$ is the chemical potential of the solvent or solute, \mathbf{v}^α is the velocity of constituent α , $f_{\alpha\beta}$ is the diffusive drag coefficient between constituents α and β (with $f_{\beta\alpha} = f_{\alpha\beta}$), and ρ^α is the apparent density of constituent α . In this treatment, the solute–solvent mixture is assumed to be dilute and ideal (solute activity coefficients and osmotic coefficients of unity) so that the constitutive relations for the solvent and solute chemical potentials

are given by

$$\tilde{\mu}^w = \mu_0^w(\theta) + \frac{1}{\rho_T^w} \left(p - R\theta \sum_{\beta \neq s, w} c^\beta \right), \quad (3)$$

$$\tilde{\mu}^\alpha = \mu_0^\alpha(\theta) + \frac{R\theta}{M_\alpha} \ln \frac{c^\alpha}{\kappa^\alpha c_0^\alpha}, \quad \alpha \neq s, w, \quad (4)$$

where c^α is the solute concentration on a solvent volume basis, M_α is the molecular weight of solute α , R is the universal gas constant and θ is the absolute temperature. Since the pore size distribution within the solid matrix may vary, solutes may not have access to all of the solvent available within the matrix due to steric volume exclusion effects. Mauck et al. (2003) extended the formulation of the solute chemical potential to account for this effect by incorporating the partition coefficient κ^α which, for an ideal solution, is the solubility of solute α inside the mixture relative to free solution. Thus c^α/κ^α is the concentration of solute per volume of accessible solvent; κ^α is assumed to be constant in this analysis. ρ_T^w is the true density of the solvent and μ_0^α is the chemical potential of constituent α in the standard state (when $c^\alpha/\kappa^\alpha = c_0^\alpha$ in the case of solutes, and when all $c^\alpha = 0$ and $p = 0$ in the case of the solvent). The solute standard state is a constant, usually taken to be $c_0^\alpha = 1$ M (Tinoco, 2002). Substituting Eqs. (3)–(4) into Eq. (2) and recognizing that $\rho^\alpha = M_\alpha \varphi^w c^\alpha$ ($\alpha \neq s, w$), and $\rho^w = \varphi^w \rho_T^w$ where φ^w is the volume fraction of the solvent in the mixture, yields

$$-\varphi^w \left(\text{grad } p - R\theta \sum_{\beta \neq s, w} \text{grad } c^\beta \right) + \sum_{\beta} f_{w\beta} (\mathbf{v}^\beta - \mathbf{v}^w) = \mathbf{0}, \quad (5)$$

$$-\varphi^w c^\alpha R\theta \frac{\text{grad } c^\alpha}{c^\alpha} + \sum_{\beta} f_{\alpha\beta} (\mathbf{v}^\beta - \mathbf{v}^\alpha) = \mathbf{0}, \quad \alpha \neq s, w. \quad (6)$$

This formulation is simplified to account for friction between solutes and the solvent and between solutes and the mixture while neglecting the solute-against-solute diffusive drag. The non-zero diffusive drag coefficients are given by (Lai et al., 1991; Gu et al., 1998; Mauck et al., 2003; Meerveld et al., 2003)

$$f_{ws} = \frac{(\varphi^w)^2}{k}, f_{w\alpha} = \frac{\varphi^w R\theta c^\alpha}{D_0^\alpha}, f_{\alpha w} + f_{s\alpha} = \frac{\varphi^w R\theta c^\alpha}{D^\alpha}, \quad (7)$$

where k is the hydraulic permeability of the solvent in the solid matrix, D^α is the solute diffusivity in the mixture and D_0^α is its diffusivity in free solution. In general, due to steric exclusion effects and tortuosity, D^α is smaller than D_0^α . From these equations we can interpret the diffusion coefficient of a solute in free solution to result only from the frictional drag of the solute with the solvent ($f_{w\alpha}$); in the presence of a solid matrix however, the diffusion coefficient results from the

frictional drag between solute and solvent and between solute and solid matrix ($f_{w\alpha} + f_{s\alpha}$). Substituting Eq. (7) into Eqs. (5)–(6) yields

$$-\text{grad } p + R\theta \sum_{\beta \neq s, w} \text{grad } c^\beta + \frac{\varphi^w}{k} (\mathbf{v}^s - \mathbf{v}^w) + \sum_{\beta \neq s, w} \frac{R\theta c^\beta}{D_0^\beta} (\mathbf{v}^\beta - \mathbf{v}^w) = \mathbf{0}, \quad (8)$$

$$-\text{grad } c^\alpha + \frac{c^\alpha}{D^\alpha} (\mathbf{v}^s - \mathbf{v}^\alpha) + \frac{c^\alpha}{D_0^\alpha} (\mathbf{v}^w - \mathbf{v}^s) = \mathbf{0}, \quad \alpha \neq s, w. \quad (9)$$

Eq. (9) can be solved for $\mathbf{v}^\alpha - \mathbf{v}^s$ in terms of $\mathbf{v}^w - \mathbf{v}^s$; substituting this result into Eq. (8) and rewriting $\mathbf{v}^\beta - \mathbf{v}^w$ as $(\mathbf{v}^\beta - \mathbf{v}^s) + (\mathbf{v}^s - \mathbf{v}^w)$, these equations can be solved simultaneously to yield

$$\varphi^w (\mathbf{v}^w - \mathbf{v}^s) = -\tilde{k} \left[\text{grad } p - R\theta \sum_{\alpha \neq s, w} \left(1 - \frac{D^\alpha}{D_0^\alpha} \right) \text{grad } c^\alpha \right], \quad (10)$$

$$\varphi^w c^\alpha (\mathbf{v}^\alpha - \mathbf{v}^s) = -\varphi^w D^\alpha \text{grad } c^\alpha + \frac{D^\alpha}{D_0^\alpha} c^\alpha \varphi^w (\mathbf{v}^w - \mathbf{v}^s), \quad \alpha \neq s, w, \quad (11)$$

where

$$\tilde{k} = \frac{1}{\frac{1}{k} + \frac{R\theta}{\varphi^w} \sum_{\alpha \neq s, w} \left(1 - \frac{D^\alpha}{D_0^\alpha} \right) \frac{c^\alpha}{D_0^\alpha}}. \quad (12)$$

$\varphi^w (\mathbf{v}^w - \mathbf{v}^s)$ is the volumetric flux of solvent relative to the solid matrix and $\varphi^w c^\alpha (\mathbf{v}^\alpha - \mathbf{v}^s)$ is the molar flux of solute α relative to the solid matrix. The material properties of the mixture include the hydraulic permeability of the solid matrix to pure solvent, k ; \tilde{k} is the hydraulic permeability of the matrix to the solution (solvent + solutes).

In addition to these momentum equations the equations of conservation of mass for the mixture as a whole and for the individual solutes are given by

$$\text{div} \left[\mathbf{v}^s + \varphi^w (\mathbf{v}^w - \mathbf{v}^s) + \sum_{\alpha \neq s, w} \varphi^\alpha (\mathbf{v}^\alpha - \mathbf{v}^s) \right] \approx \text{div} [\mathbf{v}^s + \varphi^w (\mathbf{v}^w - \mathbf{v}^s)] = 0, \quad (13)$$

$$\frac{\partial(\varphi^w c^\alpha)}{\partial t} - \text{div} \left[\varphi^w D^\alpha \text{grad } c^\alpha - \varphi^w c^\alpha \left(\mathbf{v}^s + \frac{D^\alpha}{D_0^\alpha} (\mathbf{v}^w - \mathbf{v}^s) \right) \right] = 0, \quad \alpha \neq s, w, \quad (14)$$

where, for dilute solutions, we have taken into account that the volume fraction of solutes is much smaller than that of the solvent, $\varphi^\alpha \ll \varphi^w$.

The equations presented above are generalized relations for diffusion–convection problems in deformable

porous media, where the solution is dilute. In these expressions, φ^w depends on the matrix dilatation according to

$$\varphi^w = 1 - \frac{1 - \varphi_r^w}{\det \mathbf{F}}, \quad (15)$$

where φ_r^w is the porosity in the reference configuration of zero deformation and \mathbf{F} is the deformation gradient of the solid matrix.

The general form of boundary or interface conditions applicable to mixture problems of this type are given by

$$[[\mathbf{v}^s]] \cdot \mathbf{n} = 0, \quad (16)$$

$$[[\varphi^w(\mathbf{v}^w - \mathbf{v}^s)]] \cdot \mathbf{n} = 0, \quad (17)$$

$$[[\varphi^w c^\alpha(\mathbf{v}^\alpha - \mathbf{v}^s)]] \cdot \mathbf{n} = 0, \alpha \neq s, w, \quad (18)$$

$$[[-p\mathbf{I} + \boldsymbol{\sigma}^e]] \cdot \mathbf{n} = 0, \quad (19)$$

$$\left[\left[p - R\theta \sum_{\alpha \neq w, s} c^\alpha \right] \right] = 0 \quad (20)$$

(interface permeable to solvent),

$$\left[\left[\frac{c^\alpha}{\kappa^\alpha} \right] \right] = 0 \quad (21)$$

(interface permeable to solvent and solute α),

where $[[\cdot]]$ denotes the difference, across the interface, of the quantity in the brackets, and \mathbf{n} is the unit outward normal to the interface. These equations assume that the interface is defined somewhere on the solid matrix, which is the most common case (e.g., the cell membrane surface). Note that if the boundary or interface is not permeable to solute α , then Eq. (18) is equivalent to $\varphi^w c^\alpha(\mathbf{v}^\alpha - \mathbf{v}^s) \cdot \mathbf{n} = 0$ and Eq. (21) is not applicable. Eqs. (16)–(18) are kinematic conditions that stipulate continuity of solid matrix velocity, relative solvent flux, and relative solute molar flux across the interface, respectively. Eqs. (19)–(21) represent continuity of the total traction, solvent chemical potential, and solute chemical potentials across the interface, respectively.

2.2. Mixture model for thin semi-permeable membrane

For transport across a thin membrane of thickness h , the gradients in pressure and concentration across the membrane may be represented in scalar form by $\text{grad } p \cdot \mathbf{n} \approx -\Delta p/h$ and $\text{grad } c^\alpha \cdot \mathbf{n} \approx -\Delta c^\alpha/h$, where \mathbf{n} is the unit normal to the membrane surface. In this notation, $\Delta p = p(r) - p(r+h)$, and similarly for Δc^α , where r is the coordinate direction normal to the membrane. The flux vector components normal to the membrane are given by

$$J^w = \varphi^w(\mathbf{v}^w - \mathbf{v}^s) \cdot \mathbf{n}, \quad (22)$$

$$J^\alpha = \varphi^w c^\alpha(\mathbf{v}^\alpha - \mathbf{v}^s) \cdot \mathbf{n}, \alpha \neq s, w. \quad (23)$$

Using Eqs. (10)–(11), these expressions reduce to

$$J^w = \frac{\tilde{\kappa}}{h} \Delta p - \frac{R\theta \tilde{\kappa}}{h} \sum_{\alpha \neq s, w} \left(1 - \frac{D^\alpha}{D_0^\alpha} \right) \Delta c^\alpha, \quad (24)$$

$$J^\alpha = \frac{\varphi^w D^\alpha}{h} \Delta c^\alpha + \frac{D^\alpha}{D_0^\alpha} \bar{c}^\alpha J^w, \alpha \neq s, w, \quad (25)$$

where \bar{c}^α in the last term now represents the average solute concentration in the membrane.

Evaluating the projection of the vector equation in Eq. (1) along \mathbf{n} , and reducing the resulting expression to the case of a thin spherical membrane under symmetric conditions yields

$$\Delta p - \Delta \sigma_{rr}^e - \frac{2T}{a} = 0, \quad (26)$$

where T is the surface tension in the membrane (in units of force per unit length), a is the spherical membrane radius, and σ_{rr}^e is the normal effective (elastic) stress in the radial direction.

According to the mixture formulation the concentrations c^α appearing in the above expressions refer to quantities *inside* the membrane. To express these equations using concentrations in the cytoplasm and in the external solution, boundary conditions of the form given in Eq. (21) are needed. For the interface between the membrane and cytoplasm,

$$-p + \sigma_{rr}^e = -p_i, p - R\theta \sum_{\alpha \neq s, w} c^\alpha = p_i - R\theta \sum_{\beta \neq s, w} c_i^\beta, \quad (27)$$

$$c^\alpha = \frac{\kappa^\alpha}{\kappa_i^\alpha} c_i^\alpha,$$

where p_i is the fluid pressure in the cytoplasm; c_i^α is the concentration of solute α in the cytoplasm; κ_i^α is the partition coefficient of the solute between the cytoplasm and the external solution and κ^α is the corresponding partition coefficient between the membrane and external solution. Similarly, for the interface between the membrane and external solution,

$$-p + \sigma_{rr}^e = -p_e, \quad p - R\theta \sum_{\alpha \neq s, w} c^\alpha = p_e - R\theta \sum_{\beta \neq s, w} c_e^\beta, c^\alpha = \kappa^\alpha c_e^\alpha, \quad (28)$$

where p_e is the fluid pressure and c_e^α is the concentration of solute α in the external solution. Using these relations Δp , $\Delta \sigma_{rr}^e$ and Δc^α can be evaluated from the difference, and \bar{c}^α from the mean, of the respective expressions in Eqs. (27) and (28) to yield

$$\Delta p = \frac{2T}{a} - R\theta \left[\sum_{\beta \neq s, w} (c_i^\beta - c_e^\beta) - \sum_{\alpha \neq s, w} \Delta c^\alpha \right], p_i - p_e = \frac{2T}{a}, \quad (29)$$

$$\Delta c^\alpha = \kappa^\alpha \left(\frac{c_i^\alpha}{\kappa_i^\alpha} - c_e^\alpha \right), \bar{c}^\alpha = \frac{\kappa^\alpha}{2} \left(\frac{c_i^\alpha}{\kappa_i^\alpha} + c_e^\alpha \right). \quad (30)$$

Substituting these expressions, along with Eq. (26), into Eqs. (24) and (25) produces

$$J^w = L_p \left[\frac{2T}{a} - R\theta \sum_{\alpha \neq s,w} (c_i^\alpha - c_e^\alpha) - (1 - \sigma^\alpha) \left(\frac{c_i^\alpha}{\kappa_i^\alpha} - c_e^\alpha \right) \right], \quad (31)$$

$$J^\alpha = P^\alpha \left(\frac{c_i^\alpha}{\kappa_i^\alpha} - c_e^\alpha \right) + (1 - \sigma^\alpha) \frac{1}{2} \left(\frac{c_i^\alpha}{\kappa_i^\alpha} + c_e^\alpha \right) J^w, \quad (32)$$

where

$$L_p = \frac{\tilde{k}}{h}, P^\alpha = \kappa^\alpha \frac{\varphi^w D^\alpha}{h}, \sigma^\alpha = 1 - \kappa^\alpha \frac{D^\alpha}{D_0^\alpha} \quad (33)$$

L_p is the membrane hydraulic conductivity (or conductance), P^α is the membrane permeability of solute α and σ^α is Staverman's reflection coefficient. These expressions are consistent with the physical meaning attributed to the material parameters of the K–K model (Kedem and Katchalsky, 1961). For example, Staverman's coefficient is equal to zero when the solute can diffuse through the membrane as easily as through pure solvent (no membrane resistance), $\kappa^\alpha D^\alpha = D_0^\alpha$. Conversely, if the solute cannot diffuse through the membrane, $\kappa^\alpha D^\alpha = 0$, which leads to $\sigma^\alpha = 1$ and $P^\alpha = 0$. Substituting Eqs. (30) and (33) into Eq. (12) provides an explicit dependence of L_p on the external concentrations,

$$L_p = \frac{1}{\frac{1}{L_{p0}} + R\theta \sum_{\alpha \neq s,w} \frac{(\kappa^\alpha - 1 + \sigma^\alpha)(1 - \sigma^\alpha)}{P^\alpha} \frac{1}{2} \left(\frac{c_i^\alpha}{\kappa_i^\alpha} + c_e^\alpha \right)}, \quad (34)$$

where $L_{p0} = k/h$ is the value of L_p in the absence of solutes.

Integrating the mixture continuity of mass equation in Eq. (13) and recognizing that all velocities are equal to zero at the cell center yields $J^w = \varphi^w(\mathbf{v}^w - \mathbf{v}^s) \cdot \mathbf{n} = -\mathbf{v}^s \cdot \mathbf{n}$ where \mathbf{v}^s is the velocity of the cell membrane. It follows from this result that $J^w A = -dV/dt$ where A is the cell surface area ($A = 4\pi a^2$) and V is its volume ($V = 4\pi a^3/3$). By integrating the solute continuity of mass equation in Eq. (14) over the cell volume, we find that $J^\alpha A = -dn_i^\alpha/dt$, where n_i^α is the number of moles of solute inside the cell. Substituting all these results into Eqs. (31) and (32) yields

$$\frac{dV}{dt} = -AL_p \left[\frac{2T}{a} - R\theta \sum_{\alpha \neq s,w} (c_i^\alpha - c_e^\alpha) - (1 - \sigma^\alpha) \left(\frac{c_i^\alpha}{\kappa_i^\alpha} - c_e^\alpha \right) \right], \quad (35)$$

$$\frac{dn_i^\alpha}{dt} = -AP^\alpha \left(\frac{c_i^\alpha}{\kappa_i^\alpha} - c_e^\alpha \right) + (1 - \sigma^\alpha) \frac{1}{2} \left(\frac{c_i^\alpha}{\kappa_i^\alpha} + c_e^\alpha \right) \frac{dV}{dt}. \quad (36)$$

In these expressions the internal concentrations of solutes are related to the corresponding number of moles via

$$c_i^\alpha = \frac{n_i^\alpha}{\varphi_i^w V}, \quad (37)$$

where φ_i^w is the average water content (porosity) of the cell. Furthermore, from kinematic considerations under finite deformation as given in Eq. (15),

$$\varphi_i^w = 1 - (1 - \varphi_{ir}^w) \frac{V_r}{V}, \quad (38)$$

where φ_{ir}^w and V_r are the cell water content and volume in the reference configuration (in the initial state prior to osmotic loading), respectively. Note that c_e^α for all solute species are prescribed as boundary conditions. For a non-permeating solute we have $\kappa^\alpha = 0$, which leads to $\sigma^\alpha = 1$ and $P^\alpha = 0$ according to Eq. (33), so that Eq. (36) yields $dn_i^\alpha/dt = 0$. Thus, for a non-permeating solute, n_i^α is constant (i.e., the number of moles of non-permeating solute inside the cell remains constant). Substituting Eqs. (37)–(38) into Eqs. (35)–(36) produces a set of coupled nonlinear ordinary differential equations in the unknowns $n_i^\alpha(t)$ and $V(t)$ which can be solved subject to appropriate initial conditions, given a constitutive relation between the membrane tension T and surface area A .

2.3. Permeating and non-permeating solutes

The analysis can now proceed to consider solutes which can permeate across the membrane, and solutes which cannot. For the case of one permeating ($\alpha = p$) and one non-permeating ($\alpha = n$) solute species, it follows that $J^n = 0$, so that the only remaining relations are

$$\frac{dV}{dt} = -AL_p \left(\frac{2T}{a} - R\theta \left[c_i^p - c_e^p + c_i^n - c_e^n - (1 - \sigma^p) \left(\frac{c_i^p}{\kappa_i^p} - c_e^p \right) \right] \right), \quad (39)$$

$$\frac{dn_i^p}{dt} = -AP^p \left(\frac{c_i^p}{\kappa_i^p} - c_e^p \right) + (1 - \sigma^p) \frac{1}{2} \left(\frac{c_i^p}{\kappa_i^p} + c_e^p \right) \frac{dV}{dt} \quad (40)$$

with

$$L_p = \frac{1}{\frac{1}{L_{p0}} + R\theta \frac{(\kappa^p - 1 + \sigma^p)(1 - \sigma^p)}{2P^p} \left(\frac{c_i^p}{\kappa_i^p} + c_e^p \right)}. \quad (41)$$

To evaluate the equilibrium response for the system of equations in Eqs. (39)–(40), let $dn^p/dt = 0$ and $dV/dt = 0$, which yields

$$\begin{aligned} c_i^p &= \kappa_i^p c_e^p \\ c_i^n &= c_e^n + (1 - \kappa_i^p) c_e^p + \frac{2T}{R\theta a} \text{ at equilibrium.} \end{aligned} \quad (42)$$

This equilibrium solution is equally valid in the reference state (assuming that the reference state is at equilibrium), so that

$$\begin{aligned} c_{ir}^p &= \kappa_i^p c_{er}^p \\ c_{ir}^n &= c_{er}^n + (1 - \kappa_i^p) c_{er}^p + \frac{2T_r}{R\theta a_r}, \end{aligned} \quad (43)$$

where the subscript r refers to quantities evaluated in the reference state. Substituting Eqs. (37)–(38) into the above equilibrium solutions and recognizing that the number of moles of non-permeating solute inside the cell remains constant, $n_{ir}^n = n_i^n$, produces an expression for the equilibrium values of $n_i^p(t)$ and $V(t)$,

$$\begin{aligned} n_i^p &= \frac{2T_r/R\theta a_r + c_{er}^n + (1 - \kappa_i^p) c_{er}^p}{2T/R\theta a + c_e^n + (1 - \kappa_i^p) c_e^p} \varphi_{ir}^w V_r \kappa_i^p c_e^p \\ \frac{V}{V_r} &= 1 + \left[\frac{2T_r/R\theta a_r + c_{er}^n + (1 - \kappa_i^p) c_{er}^p}{2T/R\theta a + c_e^n + (1 - \kappa_i^p) c_e^p} - 1 \right] \varphi_{ir}^w \\ &\text{at equilibrium.} \end{aligned} \quad (44)$$

Since the cell membrane tension T will generally be a function of its areal strain, the expression for V/V_r in Eq. (44) would need to be solved nonlinearly for the radius a of the cell, except in the special case when $T = 0$. Clearly the equilibrium response to osmotic loading is independent of solvent and solute transport parameters (L_p, P^p, σ^p). In addition to being a function of the initial and final concentrations of permeating and non-permeating solutes, it is dependent on the cell membrane tension, the permeating solute partition coefficient in the cytoplasm, and the water content of the cell.

Note that under hyper-osmotic loading with very high concentrations of a non-permeating solute, $c_n^e \rightarrow \infty$, the relative volume change can be used to assess the water content φ_{ir}^w (or equivalently, the osmotically inactive solid fraction, $1 - \varphi_{ir}^w$) inside the cell under the reference configuration,

$$\lim_{c_n^e \rightarrow \infty} \frac{V}{V_r} = 1 - \varphi_{ir}^w \text{ at equilibrium.} \quad (45)$$

2.4. Three-parameter Kedem-Katchalsky model

It can be noted that the above equations reduce to the classical three-parameter K–K model (L_p, P^p, σ^p) (Kedem and Katchalsky, 1958, 1961; Kleinans, 1998) if the membrane surface tension is neglected ($T = 0$) and the permeating solute partition coefficient is assumed to be unity within the cytoplasm ($\kappa_i^p = 1$).

Thus from Eqs. (31)–(32),

$$J^w = L_p(p_i - p_e) - R\theta L_p[\sigma^p(c_i^p - c_e^p) + c_i^n - c_e^n], \quad (46)$$

$$J^p = P^p(c_i^p - c_e^p) + (1 - \sigma^p) \frac{1}{2}(c_i^p + c_e^p) J^w, \quad (47)$$

where we have replaced $2T/a$ with $p_i - p_e$ as per Eq. (29) for ease of comparison. However, even in this special reduced form the hydraulic conductivity is still found to be concentration-dependent according to Eq. (41),

$$L_p = \frac{1}{\frac{1}{L_{p0}} + R\theta \frac{(\kappa^p - 1 + \sigma^p)(1 - \sigma^p)}{2P^p} (c_i^p + c_e^p)}. \quad (48)$$

This result suggests that the mixture formulation is more general than the classical phenomenological equations.

3. Results

To analyze the influence of the various material parameters on the response of a cell to osmotic loading, we propose to investigate each parameter independently of others. In contrast to the classical three-parameter K–K model, the general set of equations in (39)–(41) has five parameters, $L_{p0}, P^p, \sigma^p, \kappa^p$ and κ_i^p , in addition to the need for a constitutive relation between the membrane tension T and area A . Since the governing differential equations are nonlinear specific numerical examples are given to illustrate the influence of the parameters that are not traditionally included in the K–K model. In all cases the temperature is given by $\theta = 25^\circ\text{C} = 298\text{ K}$ and the cell radius and water content in the reference state are $a_r = 10\ \mu\text{m}$, $\varphi_{ir}^w = 0.7$. The hydraulic conductivity of the membrane at zero solute concentration is taken as $L_{p0} = 5 \times 10^{-14}\ \text{m}^3/\text{Ns}$; the solute permeability in the limit when $\kappa^p = 1$ is taken as $\varphi^w D^z/h = 5 \times 10^{-8}\ \text{m/s}$; and for simplicity it is assumed that $D^z/D_0^z = 1/2$ so that $\sigma^z = 1 - \kappa^z/2$ according to Eq. (33). Integration of the nonlinear ordinary differential equations was performed numerically using the Runge–Kutta method of order 4 (Conte and De Boor, 1980) in a custom-written program; numerical convergence was achieved in all cases.

3.1. Concentration-dependence of membrane hydraulic conductivity

When examining Eqs. (39)–(41), it can be noted that the parameter κ^p appears explicitly only in the expression for L_p in Eq. (41). If we find that the concentration-dependence of L_p has a negligible effect on the overall response of Eqs. (39)–(41), then the five-parameter model would effectively be reduced to a four-parameter model (L_{p0}, P^p, σ^p and κ_i^p). This is investigated

numerically using the following representative choice of parameters:

$$0 \leq \kappa^p \leq 1, \kappa_i^p = 1. \quad (49)$$

The response to hyper-osmotic loading with a permeable solute is analyzed, with

$$\begin{aligned} c_{er}^p &= 0 \text{ Osm}, c_e^p = 1 \text{ Osm}, \\ c_{er}^n &= 0.3 \text{ Osm}, c_e^n = 0.3 \text{ Osm}. \end{aligned} \quad (50)$$

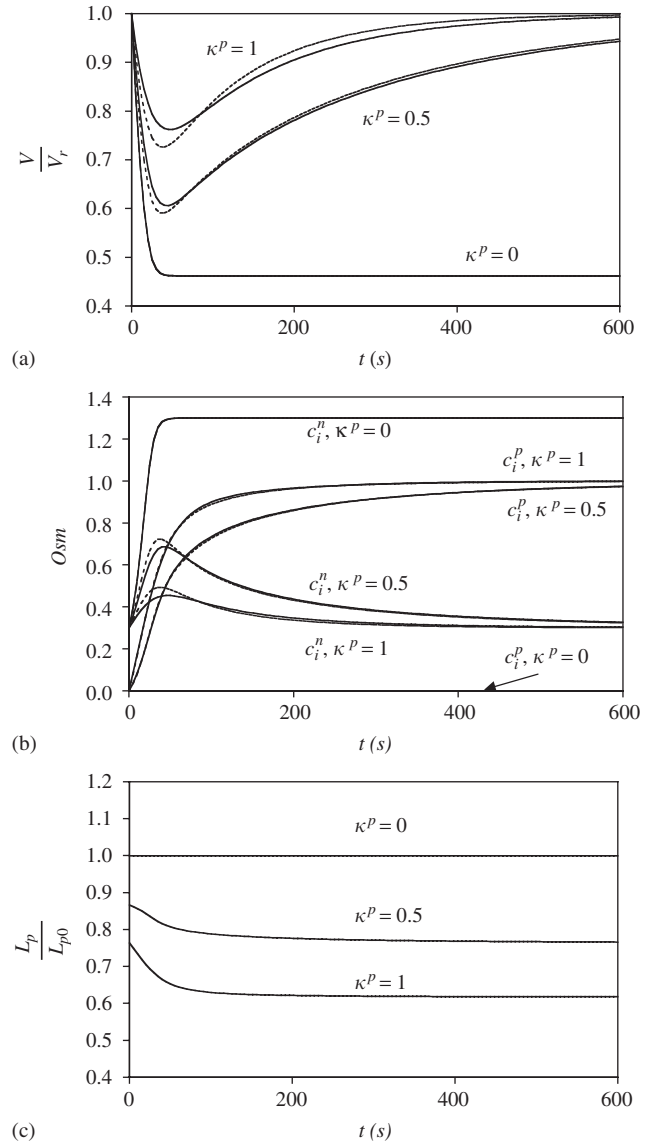


Fig. 1. Comparison of cell response to hyper-osmotic loading, when the hydraulic conductivity L_p is taken to be concentration-dependent (solid lines) [Eq. (41)] or assumed constant (dashed lines) [$L_p = L_{p0}$], for various values of the solute partition coefficient in the membrane, κ^p . The case $\kappa^p = 0$ is equivalent to hyper-osmotic loading with a non-permeating solute. (a) Relative cell volume response, V/V_r . (b) Internal concentration of permeating solute, c_i^p , and non-permeating solute, c_i^n . (c) Concentration-dependent normalized membrane hydraulic conductivity, L_p/L_{p0} .

For this analysis the membrane tension is taken as $T = 0$. The resulting cell volume response, V/V_r , is presented in Fig. 1a. For $\kappa^p = 1$ and 0.5, the volume initially decreases before recovering to its initial value at equilibrium (as also predicted from the closed-form equilibrium solution in Eq. (44)). This is the classical response to hyper-osmotic loading, whereby water initially exudes from the cell due to the higher external solute concentration; as the external permeating solute slowly diffuses into the cell however, the concentrations of permeating and non-permeating solutes inside and outside eventually balance themselves (Fig. 1b) and water flows back into the cell until there is complete volume recovery. In the limiting case of $\kappa^p = 0$ however, the solute is completely excluded from the membrane and thus cannot permeate across it. Consequently, water will exude from the cell as the volume decreases, until the decrease in volume produces a balance between the concentration of non-permeating solute inside (c_i^n) and the concentrations of permeating and non-permeating solutes outside (Fig. 1b). In this case there is no volume recovery achieved at equilibrium. The variation of the concentration-dependent L_p as a function of time is shown in Fig. 1c. When the solute can permeate across the cell membrane ($\kappa^p > 0$), the value of L_p drops significantly below that of L_{p0} , particularly when $\kappa^p = 1$. The greatest difference observed in V/V_r between concentration-dependent and constant values of L_p is thus observed at $\kappa^p = 1$ (Fig. 1a).

3.2. Effect of permeating solute partition coefficient in cytoplasm

According to the equations for the equilibrium solution, Eq. (44), the partition coefficient for the permeating solute between the cytoplasm and external solution, κ_i^p , influences the equilibrium value of V/V_r . The complete time-dependent response of a cell to hyper-osmotic loading is investigated for various values of κ_i^p , using the material parameters

$$\kappa^p = 1, 0 \leq \kappa_i^p \leq 1. \quad (51)$$

In this analysis, L_p is concentration-dependent, $T = 0$, and the external solute concentrations are given by Eq. (50). Note that the limiting case $\kappa_i^p = 0$ requires special treatment in the numerical solution since the permeating solute concentration inside the cell must reduce to zero, which is equivalent to osmotic loading with a non-permeating solute. Results show that κ_i^p has a very significant influence on the relative change in volume of the cell (Fig. 2a). Only partial volume recovery is achieved when $\kappa_i^p < 1$. The reason for this outcome is apparent from Fig. 2b, which shows that the internal concentration of permeating solute decreases with decreasing values of κ_i^p . Interestingly, as κ_i^p becomes smaller, the volume response to osmotic

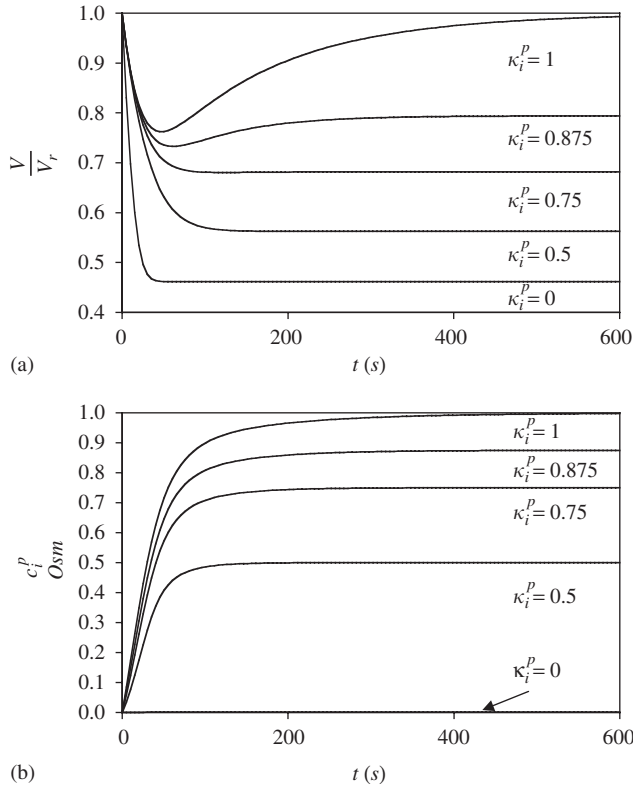


Fig. 2. Response to hyper-osmotic loading for various values of the solute partition coefficient in the cytoplasm, κ_i^p : (a) Relative cell volume V/V_r , and (b) internal concentration of permeating solute, c_i^p .

loading with a permeating solute becomes qualitatively similar to the response to loading with a non-permeating solute, as can be construed from the responses at $\kappa_i^p = 0.5$ and $\kappa_i^p = 0$ in Fig. 2a. This serves as a cautionary note in the interpretation of experimental data, namely that the lack of volume recovery following osmotic loading does not necessarily imply that the solute is non-permeating. The response shown in Fig. 2a is remarkably similar to the recent experimental study of Lucio et al. (2003).

3.3. Effect of membrane tension

To investigate the influence of membrane tension on the volumetric response, we now provide a constitutive relation between T and the areal strain. In this formulation it is assumed that the membrane is slack below a threshold value of the areal strain and supports tensile stresses above that threshold (Guilak et al., 2002),

$$T = \begin{cases} 0, & A \leq A_0, \\ K \left(\frac{A}{A_0} - 1 \right)^\beta, & A \geq A_0, \end{cases} \quad (52)$$

where A_0 is the cell surface area above which tension develops in the membrane. For simplicity in the current

analysis, it is assumed that this threshold transition point coincides with the reference configuration of the cell, $A_0 = A_r$. Thus tension will exist in the membrane under hypo-osmotic loading (swelling) relative to the reference state, but not under hyper-osmotic loading (shrinking). Furthermore, the power law of Eq. (52) is implemented in its simplest form, with $\beta = 1$. This leaves the area expansion modulus K as a parameter that can be varied in the analysis. The numerical example uses the following choice of parameters,

$$\kappa^p = 1, \kappa_i^p = 1, 0 \leq K \leq 1 \text{ N/M}. \quad (53)$$

This range of K is based on values reported for red blood cells (Evans and Waugh, 1977; Waugh and Evans, 1979) and lipid membranes (Needham and Nunn, 1990). A representative case of hypo-osmotic loading with a permeating solute is obtained with

$$\begin{aligned} c_{er}^p &= 0.3 \text{ Osm}, c_e^p = 0 \text{ Osm}, \\ c_{er}^n &= 0.3 \text{ Osm}, c_e^n = 0.3 \text{ Osm}, \end{aligned} \quad (54)$$

whereas hyper-osmotic loading is obtained with

$$\begin{aligned} c_{er}^p &= 0.3 \text{ Osm}, c_e^p = 0.6 \text{ Osm}, \\ c_{er}^n &= 0.3 \text{ Osm}, c_e^n = 0.3 \text{ Osm}. \end{aligned} \quad (55)$$

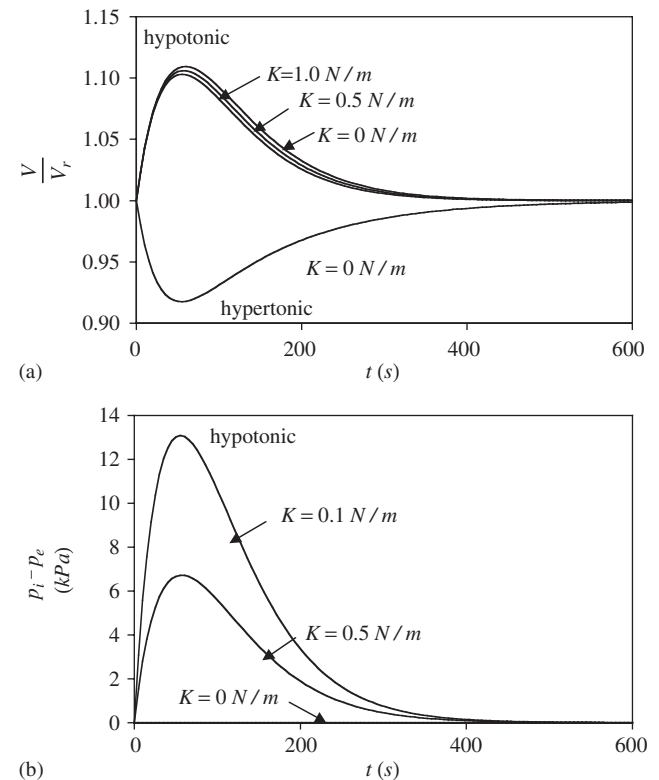


Fig. 3. Response to hyper-osmotic and hypo-osmotic loading with a permeating solute, for various values of the area expansion modulus K . Membrane tension occurs only under hypo-osmotic loading in this example. (a) Relative cell volume V/V_r , and (b) pressure difference between the inside and outside of the cell, $p_i - p_e$.

The resulting relative volume change of the cell is presented in Fig. 3a, showing an asymmetric response between hyper- and hypo-osmotic loading even in the absence of membrane tension, as supported from experiments (Curry et al., 2000). When membrane tension does develop ($K > 0$), the peak volumetric change decreases and pressure rises inside the cell as the membrane expands under hypo-osmotic loading. The pressure then returns to zero as the cell recovers its initial volume (Fig. 3b).

The response to loading with a non-permeating solute can similarly be simulated with the representative conditions

$$\begin{aligned} c_{er}^p &= 0 \text{ Osm}, c_e^p = 0 \text{ Osm}, \\ c_{er}^n &= 0.3 \text{ Osm}, c_e^n = 0.2 \text{ Osm} \end{aligned} \quad (56)$$

for hypo-osmotic loading and

$$\begin{aligned} c_{er}^p &= 0 \text{ Osm}, c_e^p = 0 \text{ Osm}, \\ c_{er}^n &= 0.3 \text{ Osm}, c_e^n = 0.4 \text{ Osm} \end{aligned} \quad (57)$$

for hyper-osmotic loading. The asymmetric volume response between hyper- and hypo-osmotic loading is even more apparent with non-permeating solutes

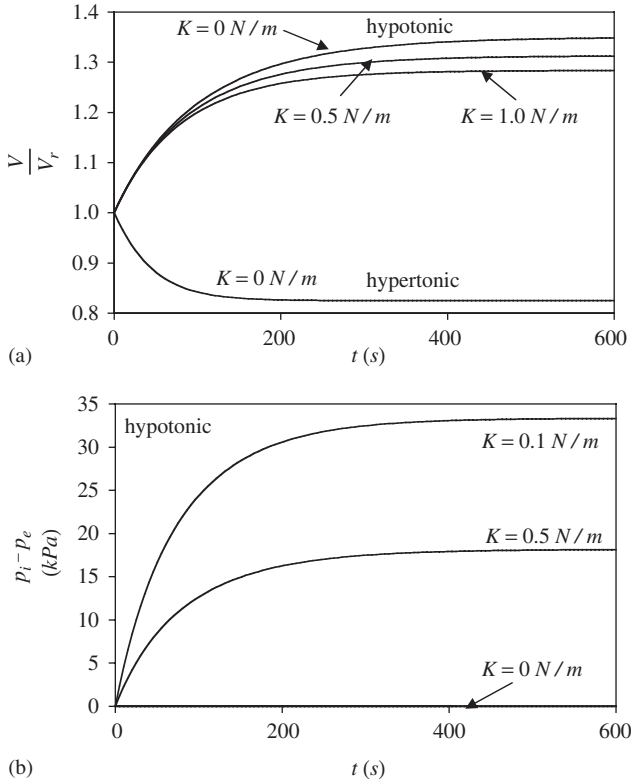


Fig. 4. Response to hyper-osmotic and hypo-osmotic loading with a non-permeating solute, for various values of the area expansion modulus K . (a) Relative cell volume V/V_r , and (b) pressure difference between the inside and outside of the cell, $p_i - p_e$.

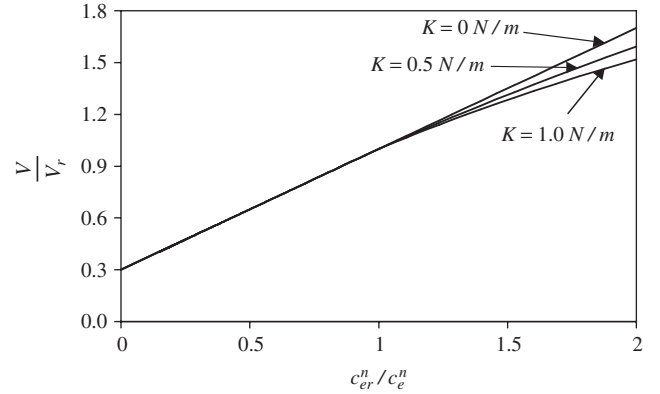


Fig. 5. Equilibrium response of V/V_r for various values of the area expansion modulus K . When $K > 0$, a transition occurs from a linear to a non-linear response at $c_{er}^n = c_e^n = 0.3 \text{ Osm}$.

(Fig. 4a). There is no volume recovery under loading with a non-permeating solute, and for $K > 0$ the internal fluid pressure remains elevated at steady-state, to balance the membrane tension (Fig. 4b). The equilibrium volume increase under hypo-osmotic loading is smaller with increasing membrane stiffness.

In addition to analyzing the transient response to osmotic loading, we can also plot the equilibrium volume change in response to osmotic loading with a non-permeating solute, as V/V_r versus c_{er}^n / c_e^n , for various values of the membrane area expansion modulus K . This is achieved by substituting the constitutive relation of Eq. (52) into the equilibrium solution of Eq. (44), for the special case $A_0 = A_r$ and $\beta = 1$,

$$\frac{V}{V_r} = \begin{cases} 1 - \phi_{ir}^w + \phi_{ir}^w \frac{c_{er}^n}{c_e^n} & A \leq A_r, c_{er}^n \leq c_e^n \\ 1 + \left[\frac{c_{er}^n}{\frac{2}{R\theta a} K \left(\frac{A}{A_r} - 1 \right) + c_e^n} - 1 \right] \phi_{ir}^w & A \geq A_r, c_{er}^n \geq c_e^n \end{cases} \quad (58)$$

where $V/V_r = (a/a_r)^3$ and $A/A_r = (a/a_r)^2$. Under hypo-osmotic loading ($c_{er}^n \geq c_e^n$), this is a non-linear equation in the unknown cell radius a . For a reference configuration $c_{er}^n = 0.3 \text{ Osm}$, the equilibrium response V/V_r is plotted against c_{er}^n / c_e^n in Fig. 5. When there is no membrane tension, the response is linear and corresponds to the classical Boyle-van't Hoff relation or Ponder plot, which has been confirmed experimentally (Guilak et al., 2002; Xu et al., 2003). According to Eq. (58) the slope of the line is ϕ_{ir}^w and the intercept at the origin is $1 - \phi_{ir}^w$. In the presence of membrane tension however, the response becomes nonlinear, with tapering off of the volume increase under hypo-osmotic loading.

4. Discussion

Mixture theory has been used to formulate the equations for osmotic loading of a fluid-filled spherical membrane representative of a cell. The fundamental principles of mixture theory represent a generalization of the phenomenological equations that are based on irreversible thermodynamics (Onsager, 1931a, b; Staverman, 1952). The mixture theory equations, Eqs. (10)–(12), are not limited to thin membranes but are applicable to any continuum consisting of a mixture of a neutral solid, solvent, and solute constituents. The material parameters appearing in these equations are the familiar properties of transport theory, including the permeability of the solvent through the porous solid matrix, and the diffusivities of the solutes in the mixture and in free solution. By reducing these governing equations to the special case of a spherically shaped thin membrane a formulation was obtained which is a generalized form of the classical K–K equations. Equivalences were established between the material parameters of mixture theory and the classical phenomenological parameters, as presented in Eq. (33). These equivalences are intuitive and consistent with the physical interpretations attributed to the phenomenological parameters (Kedem and Katchalsky, 1961). They are also comparable to the relations presented by Gu et al. (1993), though it should be noted that these authors included charge effects, which allows them to model the membrane potential, while neglecting the friction between solutes and the solid matrix ($f_{sz} = 0$). One noteworthy generalization over the K–K model is the formulation of a concentration-dependent membrane hydraulic conductivity as shown in the general expression of Eq. (34) and in the special case of Eq. (48). The dependence of L_p on concentration has been alluded to in previous studies (Williams and Comper, 1990), though we believe that the explicit dependence derived from mixture theory in this study has not been previously reported. Another generalization relative to the K–K model is the incorporation of surface tension in the reduction to a thin spherical membrane (Evans et al., 1976).

The requisite interface boundary conditions of Eqs. (16)–(21) were applied to the mixture formulation to investigate the cell response to osmotic loading. One particular feature which bears note is the incorporation of a partition coefficient for solutes in the mixture, relative to free solution. The resulting governing equations for osmotic loading of a fluid-filled membrane, Eqs. (31)–(32), are more general than the three-parameter K–K model, Eqs. (46)–(47), though they can be reduced to that model in the limit when the cytoplasm partition coefficient for permeating solutes is equal to unity and the membrane tension is neglected.

An assumption which is implicit in the current model as well as the K–K model is that the diffusion of solutes within the cytoplasm occur at time scales significantly shorter than the transport of solutes and solvents across the membrane. Therefore homogeneous distributions of solute concentration are assumed inside the cell. The mixture formulation assumes the existence of a solid matrix in the cell (the osmotically inactive volume) since the intracellular (osmotically active) water content (ϕ_1^w) can be less than 100% and the solute partition coefficient (κ_1^s) can be less than unity. However the stiffness of this matrix, and resistance to intracellular flow through the matrix, are neglected in the current formulation, under the assumption that the magnitude of osmotic pressure developing inside the cell (e.g., Figs. 3b and 4b) is considerably higher than the stress magnitudes resulting from matrix strains, and resistance to water and solute transport across the cell membrane is significantly greater than for intracellular transport.

The numerical examples investigated in this study suggest that the concentration-dependence of the membrane hydraulic conductivity, L_p , can be significant, particularly when the membrane partition coefficient for the permeating solute, κ^p , is close to unity (Fig. 1). However, when osmotic loading is performed with a non-permeating solute, L_p remains constant and equal to L_{p0} (Fig. 1c), as is apparent from Eqs. (41) and (48) with $c_1^p = c_e^p = 0$. This observation suggests that, experimentally, L_{p0} can be determined by osmotic loading with a non-permeating solute.

The theoretical predictions of this model are in very good agreement with experimental results available in the literature. For example, the response to hyperosmotic loading with a permeating solute, as shown in Fig. 1 for the case $\kappa^p \neq 0$ agrees very well with the experiments of Xu et al. (2003) where bovine chondrocytes were osmotically loaded with glycerol (Fig. 6a). The asymmetric response to hyper- and hypo-osmotic loading with a non-permeating solute predicted in Fig. 4 is very similar to the experiments of Curry et al. (2000) who performed osmotic loading of rabbit spermatozoa (Fig. 6b). It is also interesting that varying the partition coefficient of the permeating solute in the cytoplasm can produce partial volume recoveries (Fig. 2) which are remarkably similar to experimental measurements by Lucio et al. (2003) in kidney cells treated with various doses of vasopressin hormone (Fig. 6c). This agreement suggests that the role of the partition coefficient in osmotic loading of cells may be quite significant and should be investigated in greater detail. Quantitative differences in the time scales and magnitude of volume changes between these experimental studies and the theoretical predictions of the current study are simply due to differences in cell sizes (radius a) and choices of material coefficients (L_p and P^p) and boundary conditions (values of c_e^p and c_e^s).

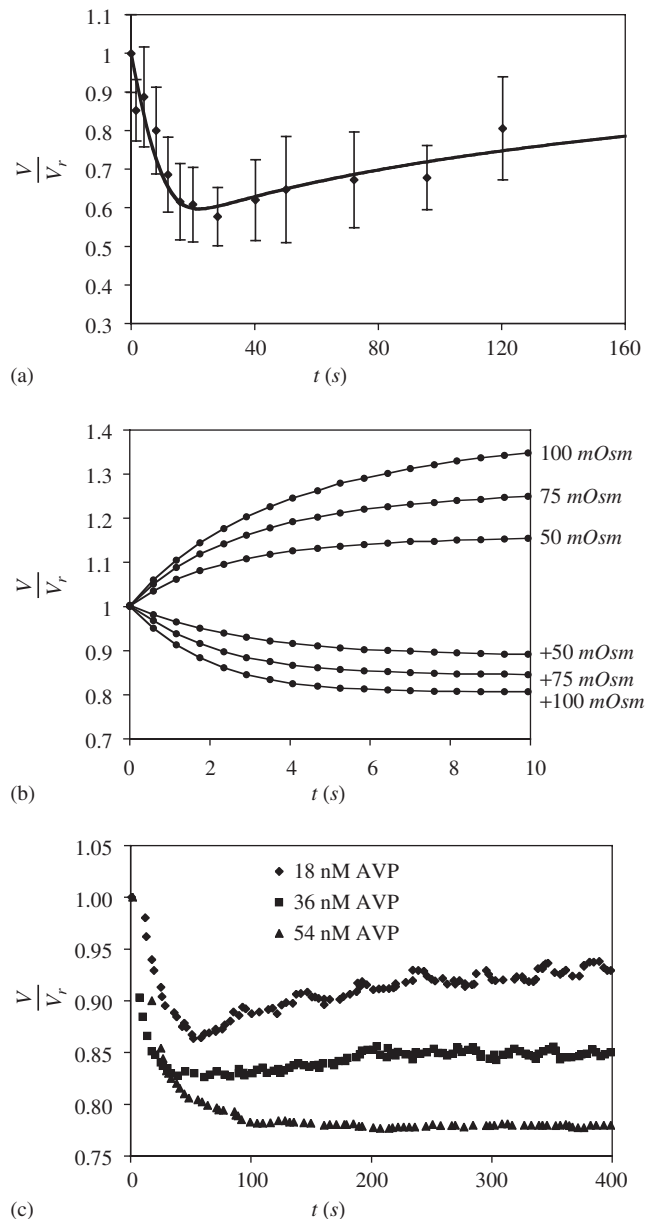


Fig. 6. (a) Hyper-osmotic loading of bovine chondrocytes with a permeating solute (1.4M glycerol) at 21 °C, with solid curve representing prediction from K–K model (Reprinted from Xu et al., 2003 Copyright (2003), with permission from The Institute of Engineering and Physics in Medicine); (b) Osmotic loading of rabbit spermatozoa at 25 °C with non-permeating solutes (sucrose for hyper-osmotic loading and dilution of cell culture media with distilled water for hypo-osmotic loading) (Reprinted from Curry et al., 2000 Copyright (2000), with permission from Elsevier); (c) Hyper-osmotic loading of Madin Darby canine kidney cell with sodium chloride in the presence of different concentrations of the hormone vasopressin, at 25 °C (Reprinted figure with permission from Lucio et al., 2003 Copyright (2003) by the American Physical Society).

Finally, the numerical simulations incorporating cell membrane elasticity show that surface tension can have a non-negligible influence on the volumetric response to osmotic loading (Figs. 3 and 4). Experimental

measurements of the equilibrium response to loading with a non-permeating solute at various concentrations may be used to infer the membrane's area expansion modulus if the Boyle–van't Hoff relationship is found to significantly deviate from a straight line under hypo-osmotic loading (Fig. 5). For bovine chondrocytes, measurements to date demonstrate a linear relationship (Guilak et al., 2002; Xu et al., 2003) more akin to the case $K = 0 \text{ N/m}$ ("perfect osmometer") in Fig. 5, suggesting that membrane tension may be negligible for those cells.

Acknowledgements

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